

Convection resistance

$$q_{\text{Convection}} = h A (T_w - T_{\infty})$$

$$q_{\text{Convection}} = \frac{(T_w - T_{\infty})}{\frac{1}{h A}}, \quad \frac{1}{h A} \text{ terms becomes the convection resistance}$$

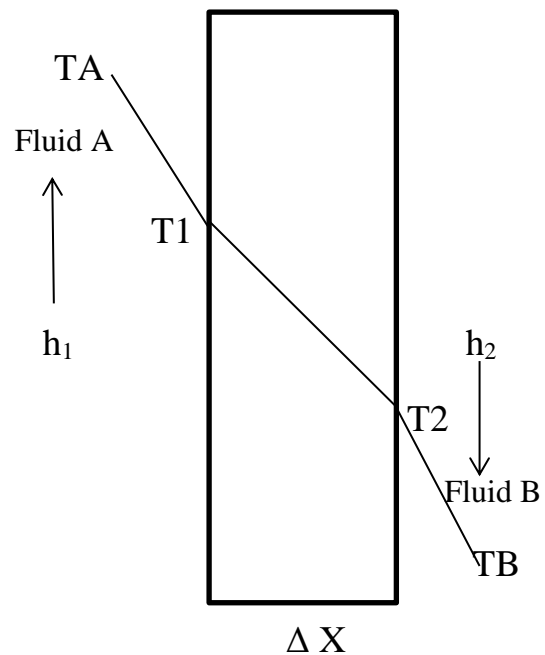
The overall heat transfer coefficient

Consider the plane wall shown in figure to a hot fluid A on one side and cooler fluid B on other side:

$$q = h_1 A (T_A - T_1)$$

$$q = \frac{(T_1 - T_2)}{\frac{\Delta X}{KA}}$$

$$q = h_2 A (T_2 - T_B)$$



$$q = \frac{(T_A - T_B)}{\frac{1}{h_1 A} + \frac{\Delta X}{KA} + \frac{1}{h_2 A}}$$



The overall heat transfer by combined conduction and convection is expressed in terms at an overall heat transfer coefficient (U) defined by :

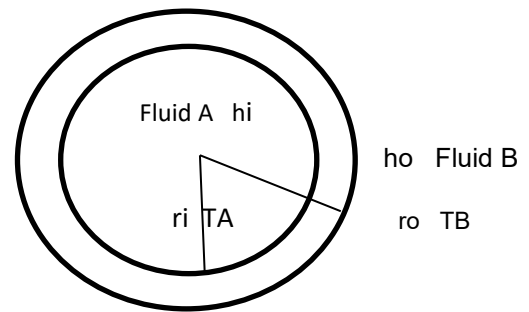
$$q = U A \Delta T_{(\text{overall})}$$

$$q = U A (T_A - T_B)$$

$$U A = \frac{1}{\frac{1}{h_1 A} + \frac{\Delta X}{KA} + \frac{1}{h_2 A}} \rightarrow U = \frac{1}{\frac{1}{h_1} + \frac{\Delta X}{K} + \frac{1}{h_2}} = \frac{1}{R_{\text{total}}}$$

For a hollow cylinder exposed to convection on its inner and outer surface as shown in figure below the heat rate (q) is calculated:

$$q = \frac{(T_A - T_B)}{\frac{1}{h_i A_i} + \frac{\ln\left(\frac{r_o}{r_i}\right)}{2\pi K L} + \frac{1}{h_o A_o}}$$



The area of convection is not the same, the terms A_i , A_o represent the inside and outside surface area of the tube. The overall heat transfer coefficient may be based on either inside or outside area of the tube.

$$U_i = \frac{1}{\frac{1}{h_i} + \frac{A_i \ln\left(\frac{r_o}{r_i}\right)}{2\pi K L} + \frac{A_i}{A_o} \frac{1}{h_o}} \quad (\text{Inside overall heat transfer coefficient})$$

$$U_o = \frac{1}{\frac{A_o}{A_i} \frac{1}{h_i} + \frac{A_o \ln\left(\frac{r_o}{r_i}\right)}{2\pi K L} + \frac{1}{h_o}} \quad (\text{Outside overall heat transfer coefficient})$$

Note: $A_i = 2 \pi r_i L$,

$$A_o = 2 \pi r_o L$$

Example:

A 0.5 ft thick of concrete wall having $k = 0.5 \text{ Btu /h.ft. } ^\circ\text{F}$ is exposed to air at 70°F ($h_i = 2 \text{ Btu /h.ft}^2 \cdot ^\circ\text{F}$) and air at 20°F ($h_o = 10 \text{ Btu /h.ft}^2 \cdot ^\circ\text{F}$) on the opposite side. Determine the heat transfer rate per unit area.

Solution

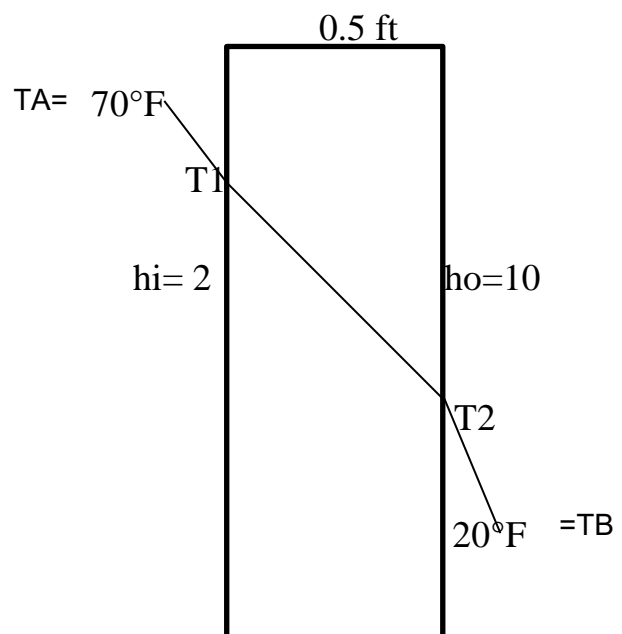
$$q = U A (T_A - T_B)$$

$$q / A = U (T_A - T_B)$$

$$q / A = \frac{1}{\frac{1}{h_i} + \frac{\Delta X}{K} + \frac{1}{h_o}} (T_A - T_B)$$

$$q / A = \frac{1}{\frac{1}{2} + \frac{0.5}{0.5} + \frac{1}{10}} (70 - 20)$$

$$= 31.25 \text{ Btu/h.ft}^2$$



Example:

Water flows at 50°C inside a 2.5-cm-inside-diameter tube such that $h_i = 3500 \text{ W/m}^2 \cdot ^\circ\text{C}$. The tube has a wall thickness of 0.8 mm with a thermal conductivity of $16 \text{ W/m} \cdot ^\circ\text{C}$. The outside of the tube loses heat by free convection with $h_o = 7.6 \text{ W/m}^2 \cdot ^\circ\text{C}$. Calculate the overall heat-transfer coefficient in the outside tube and heat loss to surrounding air at 20°C. Take the length is 1 m

Solution.

$$r_i = 1.25 \text{ cm} = 0.0125 \text{ m}$$

$$r_o = r_i + 0.8 \times 10^{-3} = 0.0133 \text{ m}$$

$$q = U_o A (T_A - T_B)$$

$$U_o = \frac{1}{A_o \cdot R_{total}}$$

$$R_1 = \frac{1}{h_i A_i}$$

$$= \frac{1}{3500 \cdot 2 \cdot \pi \cdot 0.0125 \cdot 1} = 0.00364$$

$$R_2 = \frac{\ln\left(\frac{r_o}{r_i}\right)}{2\pi K L}$$

$$= \frac{\ln\left(\frac{0.0133}{0.0125}\right)}{2 \cdot \pi \cdot 16 \cdot 1} = 0.00062$$

$$R_3 = \frac{1}{h_o A_o}$$

$$= \frac{1}{7.6 \cdot 2 \cdot \pi \cdot 0.0133 \cdot 1} = 1.575$$

$$U_o = \frac{1}{A_o \sum R} = \frac{1}{(2 \cdot \pi \cdot 0.0133 \cdot 1)(0.00364 + 0.00062 + 1.575)}$$

$$= 7.577 \text{ W/m}^2 \cdot ^\circ\text{C}$$

$$q = U_o A_o (T_A - T_B)$$

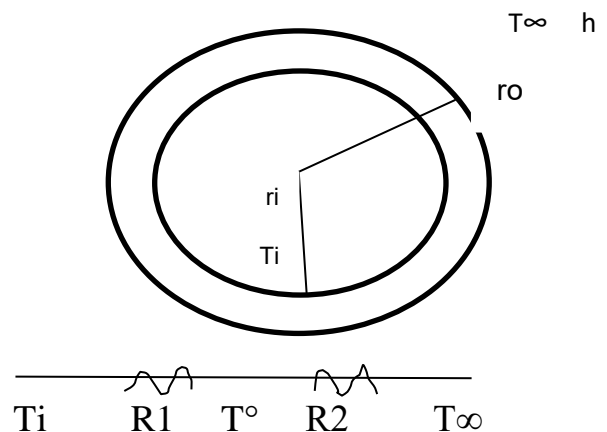
$$= 7.577 \cdot 2 \cdot \pi \cdot 0.0133 \cdot 1 \cdot (50 - 20) = 19 \text{ W}$$

Critical thickness of insulation

The wall insulation is required in various process equipment, reactors, pipelines ...etc to minimize heat loss between the system and environment. Consider a layer of insulation which might be installed around circular pipe as shown in figure the inner temperature of the insulation is T_i and the outer surface is exposed to a convection environment T_∞

$$q = \frac{(T_i - T_\infty)}{\frac{\ln\left(\frac{r_o}{r_i}\right)}{2\pi K L} + \frac{1}{2\pi r_o L h}} \quad \text{or}$$

$$q = \frac{2\pi L (T_i - T_\infty)}{\frac{\ln\left(\frac{r_o}{r_i}\right)}{K} + \frac{1}{r_o h}}$$



To determine the outer radius of insulator r_o , which will maximize the heat transfer. The maximization condition is

$$\frac{dq}{dr_o} = \frac{-2\pi L (T_i - T_\infty) \frac{1}{K r_o} + \frac{1}{h r_o^2}}{\left\{ \frac{\ln\left(\frac{r_o}{r_i}\right)}{K} + \frac{1}{r_o h} \right\}^2} \longrightarrow$$

$$r_o = \frac{k}{h} = r_c \text{ (critical radius)}$$

Example:

Calculate the critical radius of insulation for asbestos [$k = 0.17 \text{ W/m} \cdot ^\circ\text{C}$] surrounding a pipe and exposed to room air at 20°C with $h = 3 \text{ W/m}^2 \cdot ^\circ\text{C}$. Calculate the heat loss per unit length from a 200°C , 5.0-cm-diameter pipe when covered with the critical radius of insulation and without insulation.

Solution:

With insulation

$$r_o = \frac{k}{h}$$
$$= \frac{0.17}{3} = 0.0567 \text{ m} = 5.67 \text{ cm}$$

$$\frac{q}{L} = \frac{2\pi(T_i - T_\infty)}{\frac{\ln\left(\frac{r_o}{r_i}\right)}{K} + \frac{1}{r_o h}}$$
$$\frac{q}{L} = \frac{2\pi(200 - 20)}{\frac{\ln\left(\frac{0.0567}{0.025}\right)}{0.17} + \frac{1}{3 * 0.0567}} = 105.7$$

Without insulation

$$\frac{q}{L} = h A (T_w - T_\infty)$$
$$= h * 2 * \pi * r_i * (T_w - T_\infty)$$
$$= 3 * 2 * \pi * 0.025 * (200 - 20) = 84.8 \text{ w/m}$$